

### Next Generation Wastewater System for NASA

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# What's the big deal about water in space?

- \$10,000 a pound to deliver an item to the space station
- \$83,000 per gallon of water
- Water is 92 % of living costs in space
- Bottle of water (16 oz) costs \$10,000 in space!



# If you could use "space water" to pay for things

- You could fund the Federal government (\$3.8T) for a year with 46 million gallons of water (less than half of what HRSD treats each day)!
- You could be a "water millionaire" by owning 15 gallons of water!
- Or you could send your kid to college with a few liter bottles of water for room board and tuition!







### Facts about the International Space Station

- Announced during Reagan's 1984 State of the Union Address.
- First module launched in 1998; continuously occupied since 2000.
- Five different space agencies representing 15 countries built the \$100billion International Space Station and continue to operate it today.



### Water and the International Space Station

- Feces is separated out from recycling system and is released in spent containers to burn up in the earth's atmosphere.
- Typical crew size is 4 to 6; each person consumes approximately 3 gallons (11 liters) per day.
- Urine is treated through vacuum distillation via the Urine Processing Assembly (UPA).
- Water Processing Assembly (WPA) filters UPA water, condensate, and other sources.
- Russian side of station does not treat urine they send it to the Americans.



### How much water is needed?

- Each astronaut requires about 3 gallons per day
- The current recycling system is able to recycle about 85% of the wastewater generated
- Approximately 444 gallons of additional water is needed each year at a cost of \$43 million a year



444 gallons is 8 barrels, each valued at \$5 million!

### Recycling efficiency is extremely important!

- Improving recycling from 85% to NASA's goal of 95% will reduce annual resupply costs by \$24M!
- Difficult to increase mechanical/chemical recycling efficiency by 10% without excessive energy usage and consumables.
- A biological system removing organic carbon and nitrogen could permit the use of reverse or forward osmosis to achieve the target of 95% recycling.

# **Overview of Project**

- NASA's Requirements
- Current wastewater technology
- Anammox
- Pancopia's Phase I feasibility testing
- Results of Phase I research
- Phase II research and current status
- What next?

### NASA's Requirements

- System to precondition wastewater to make is suitable for final filtration use RO or FO
  - Wastewater high in ammonia (about 600 mg/l as N) and an organic carbon (about 900 mg/l COD)
  - Target removal of between 85% to 95% N and TOC
- Low level of consumables
- Shut down for long periods of time (up to a year)
- Start up quickly and reliably (less than 45 days; preferably 15 days)

### Current nitrogen removal technology (95%+ WWTPs that remove nitrogen use this or similar technology)

#### **Conventional Nitrification-Denitrification**



#### Advantages:

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 Current system being tested for past decade (membrane aerated system)

#### **Challenges for NASA:**

- Requires high levels of energy (O<sub>2</sub>)
- Requires additional carbon
- High O<sub>2</sub> requirements could cause phase flow problems in microgravity

# Nitrogen removal with anammox

- ANaerobic AMMonia OXidizing Bacteria.
- Predicted in 1977 by Broda.
- Discovered in 1995 at a plant that was removing ammonia but shouldn't have been.
- Delayed discovery due to long reproduction time (2 to 3 weeks) and highest concentrations of organisms are in inaccessible locations (deep ocean upwellings).
- Deammonification is a nascent technology(<100 plants in 2014) but can remove nitrogen for 1/3 of current costs!
- Adoption has been delayed by:
  - limited supply of organisms
  - advanced control requirements more suitable for larger plants (both problems are being worked on!)

# Deammonification with Anammox

#### Partial Nitritation-Anammox = "Deammonification"

#### ANAMMOX

"Anaerobic" Ammonia Oxidation - (New Planctomycete - Strous et al, 1999)

NH<sub>4</sub><sup>+</sup> + 1.32 NO<sub>2</sub><sup>-</sup> + 0.066 HCO<sub>3</sub><sup>-</sup> + 0.13 H<sup>+</sup> →

 $0.26 \text{ NO}_3$  +  $1.02 \text{N}_2$  +  $0.066 \text{ CH}_2 \text{O}_{0.5} \text{N}_{0.15}$  +  $2.03 \text{ H}_2 \text{O}_{0.5}$ 



#### Advantages for NASA:

- Very low energy costs (less aeration needed) and low biosolids production
- Lower O<sub>2</sub> requirements
   could help resolve phase
   flow problems related to
   microgravity

#### Challenges for NASA:

- Does not remove organic carbon
- Requires high level of control

· No additional alkalinity required

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# Treatment system used for NASA bioreactors



Use of three sets of organisms, nitrifiers, denitrifiers, and anammox to remove both carbon and nitrogen

#### Advantages :

- Low energy costs (less aeration) and low biosolids production
- Lower O<sub>2</sub> requirements could help resolve phase flow problems related to microgravity

#### Challenges for NASA:

• The ability to balance these three sets of organisms is relatively untested

# Phase I feasibility testing

- Six reactors
- Three sets of two
- Each set:
  - One reactor with organisms poured into reactor
  - One reactor with organisms embedded in the scaffold
- One set (R1/R2) test for induced dormancy for >45 days
- Two sets (R3/R4 and R5/R6) using lyophilized organisms



# Phase I Bioreactors

- Fourteen liter volume with continuous mixing (two mixers) and intermittent aeration (two airstones)
- Continuous video monitoring
- Continuous DO, T, pH, ORP, and TDS monitoring
- Daily testing of NH<sub>4</sub><sup>+</sup>, NO<sub>3</sub><sup>-</sup>, NO<sub>2</sub><sup>-</sup>, and COD



### Phase I Bioreactors



### Phase I Bioreactor Testing Protocol

- 1. Start each tank with half-strength Early Planetary Base (EPB)wastewater (WW generated on space station)
  - EPB approx. 600 mg/l NH<sub>4</sub>-N and 900 mg/l COD
- 2. No EPB addition until half N and C consumed
- 3. Feed full strength EPB until steady state (SS) reached
- 4. Test for 15 days once steady state is reached

For induced dormancy (R1/R2):

• Startup, reach SS, induce dormancy, restart, reach SS, 15 day test

For lyophilized testing (R3/R4 and R5/R6):

• Startup, reach SS, 15 day test

# Bioreactor R1: Adding nitrifiers



# Bioreactor R1: 9 days after starting



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### Bioreactor R1: Scaffold stored (47 days) for induced dormancy



### Bioreactor R1: Post-dormancy



### Bioreactor R1: Post-dormancy (video monitoring)



### R1 Data (Induced Dormancy, organisms added to reactor)

#### Phases:

- A 12 days startup
- B-25 days steady state
  - 85% NH<sub>4</sub><sup>+</sup> removal
  - 80% COD removal
- C 47 days dormancy
- D 19 days reacclimatization
- E 15 days steady state
  - 95%  $NH_4^+$  removal
  - 92% COD removal



Day of Operation

### Bioreactor R2: Embedment of organisms in scaffold



### Bioreactor R2: Scaffolds with embedded organisms



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### R2 Data (Induced Dormancy, organisms embedded in scaffold)

**Phases:** A – 12 days startup B – 25 days steady state • 80% NH<sub>4</sub><sup>+</sup> removal 78% COD removal C - 47 days dormancy D – 19 days reacclimatization E - 15 days steady state • 94%  $NH_4^+$  removal • 88% COD removal



### R3/R4/R5/R6 Lyophilized Anammox



### R3/R4/R5/R6 Reconstituted Lyophilized Organisms



### R3: 17 days after startup



### R4: 17 days after startup



### R3 Data (Lyophilized, organisms added to reactor)

#### Phases:

- A 18 days startup
- B 21 days acclimation
- C 15 days steady state
  - 88% NH<sub>4</sub><sup>+</sup> removal
  - 79% COD removal





R3 N Removal:

### R4 Data (Lyophilized, organisms embedded in scaffold)

Phases:

- A 18 days startup B - 23 days acclimation
- C 15 days steady state
  - 93% NH<sub>4</sub><sup>+</sup> removal
  - 82% COD removal



### R5/R6: Second set of lyophilized reactors

- 1. Reconstituted lyophilized organisms but did not remove all of the cryoprotectant (skim milk)
- 2. Bioreactor R5 was particularly affected and did not begin to treat EPB wastewater for two weeks
- 3. Bioreactor R5 also had levels of organic carbon and nitrogen significantly higher than the EPB wastewater contained. This was due to organic matter in the cryoprotectant.

### R5/R6: 1 and 8 days after startup



#### **Bioreactor R5**

#### Bioreactor R6



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### R5/R6: 14 and 42 days after startup



#### **Bioreactor R5**

**Bioreactor R6** 



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### Comparison of R5/R6 Data (Incomplete removal of cryoprotectant in R5)



### R5 Data (Lyophilized, organisms added to reactor)

### Phases:

- A 18 days startup
- B 7 days acclimation
- C 15 days steady state
  - 80% NH<sub>4</sub><sup>+</sup> removal
  - 75% COD removal



### R6 Data (Lyophilized, organisms embedded)

### Phases:

- A-9 days startup
- B 16 days acclimation
- C 15 days steady state
  - 88% NH<sub>4</sub><sup>+</sup> removal
  - 85% COD removal



### Phase I research results

- Five of the 6 reactors surpassed the ammonia removal/transformation criteria of 85%
- Three of the 6 reactors surpassed the organic carbon removal criteria of 85%
- All reactors removed at least 75% of ammonia and organic carbon
- All reactors met the criterion of successful startup in less than 45 days

### Phase II research and current status

Three Tasks
1. Optimize lyophilization
2. Construct reactor suitable for use in space
3. Develop operations manual for system

# Phase II, Task 1: Optimize Lyophilization

- Test 4 cryoprotectants and 4 methods of lyophilization
- Select two best combinations for further testing
- Test lyophilizing organisms and lyophilizing scaffolds with biofilms



# Phase II, Task 2: Bioreactors for Microgravity

- 35-L capacity with 5 scaffolds (1"x10"x10")
  Recirculation loop (used to add influent, maintain temp, measure DO, pH, temp, Redox, Conductivity)
- Effluent loop

(used to add dissolved oxygen, extract effluent, measure TOC, COD,  $NH_4^+$ ,  $NO_3^-$ ,  $NO_2^-$ )



# Phase II, Task 3: Develop operations manual

- 1. Run bioreactor for one year varying:
  - Temperature
  - Oxygen
  - pH
  - Feed and feed rate

#### 2. Develop Operations manual



# What Next?

- Adapting technology to small decentralized wastewater systems and septic tanks
- Developing a retrofit for small wastewater systems to upgrade secondary treatment to also remove nitrogen in one unit



# What Next?

- Adapting and applying technology for use in developing countries
- Applying technology to treat animal waste such as swine lagoons
- Coupling technology with other energy saving and resource recovery systems





# **Project Team and Partners**



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#### **Coauthors and Partners**





Dr. Karen Pickering (NASA project manager and technical resource)

Dr. Matias Vanotti (Sr. Consultant and provided nitrifiers and anammox &lab analyses)



Dr. Charles Bott, PE (Sr. Consultant; also Andy Nelson /HRSD York River WWTP provided denitrifiers)



Dr. Kevin Gilmore, PE (Primary Sr. Consultant; also for reactor design, operation, and data analysis)

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